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	Surcharge of \$ for furnish claimed priority date (37 CFR 1		or declaration later than □20	□ □ 30 mos. from the earliest \$130 00	
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	Reduction by ½ for filing by sma	all entity, if applicable. Affi	davits must be filed also. (No	ote 37 CFR 1.9, 1.27, 1.28.)	
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		nishing the English Translat	ion later than □20 □30 mos.	SUBTOTAL from the earliest claimed priority \$130 00	1,100 00
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.   An oath o	r declaration of the inventor (35 U.S.C. 371(c)(4)).
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a. □ before to b. ■ after put c. □ after 20 d. □ after 22 Note: Per months claimed e. □ by 30 m the earlif. □ after 30 by the 1 g. □ after 32 Note: Per months claimed 2. At the time	checked items are being transmitted the 18th month publication. delication and the Article 20 communication but before 20 months from the priority date. months but before 22 months (surcharge and/or processing fee included). months (surcharge and/or processing fee included). etition to revive (37 C.F.R. 1.137(a) or (b)) is necessary if 35 U.S.C. 371 requirements submitted after 22 and no proper demand for International Preliminary Examination was made by 19 months from the earliest priority date.  nonths and a proper demand for International Preliminary Examination was made by the 19th month from eest claimed priority date. months but before 32 months and a proper demand for International Preliminary Examination was made 9th month from the earliest claimed priority date (surcharge and/or processing fee included). months (surcharge and/or processing fee included). etition to revive (37 C.F.R. 1.137(a) or (b)) is necessary if 35 U.S.C. 371 requirements submitted after 32 and a proper demand for International Preliminary Examination was made by 19 months from the earliest priority date.  of transmittal, the time limit for amending claims under Article 19 ired and no amendments were made. yet expired.
3. □ Certain r	equirements under 35 U.S.C. 371 were previously submitted by the applicant on, namely:
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4/PARTS

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## SPECIFICATION

## METHOD OF PRODUCING COKE FOR METALLURGY

#### TECHNICAL FIELD

This invention relates to a method of producing coke for metallurgy, and more particularly proposes a method of producing high-strength coke for metallurgy capable of using in a large size blast furnace by blending a great amount of brand coal near to quality of a coal blend for the charge in a coke oven to form the coal blend consisting of only a few brands of coals without blending many brands of coals.

#### BACKGROUND ART

In case of making molten iron in a blast furnace, it is first necessary that iron ores and coke are alternately charged into the blast furnace and filled therein in form of layers, and these iron ore and coke are heated by hot air of high temperature blown through a tuyere and at the same time the ore is reduced to iron by CO gas generated through combustion of coke.

In order to stably conduct the operation of such a blast furnace, it is required to ensure air permeation and liquid permeation in the furnace, and hence it is inevitable to use coke having excellent properties such as strength, particle size, strength after reaction and the like. Among them, the strength (drum strength) is considered to be an important property.

In the production of such coke for the blast furnace, it is required to carbonize the coal blend (charging coal) for charging into a coke oven having constant coking property and coalification degree. For this purpose, a raw coal having a good quality (which is

mainly called by a production area, and is called as a brand) is necessary. Recently, such brands of coals (hereinafter referred to as a raw coal simply) is difficult to be get in a great amount. Therefore, there has been used so-called the coal blend obtained by blending many kinds of the raw coals having different properties in accordance with production country and production area (usually 10~20 brand coals).

In such the coal blend, it is common to blend coal of one brand in an amount of not more than 20 wt% at most. This blending thought lies in that the raw coals are blended so that a quality of coke obtained by carbonization of the coal blend in a coke oven is made to not less than a certain level. For example, it is enough to balancedly blend fibrous components forming a skeleton of coke (which is evaluated by the coalification degree of coal using volatile component, C wt%, vitrinite reflectance and the like as an indication) with coking component forming aggregate through coking of coal particles (there are fluidity of coal, expansion degree, tackiness index and the like as an indication). That is, the strength of coke after carbonization is guessed by calculating the quality as the coal blend based on coalification degree and coking property of each brand of raw coals.

At the present, 10~20 brands of raw coals are usually blended as a coal (coal blend) charged into the coke oven used for the production of coke for blast furnace. According to this method, the influence of the properties of the raw coal per one brand upon the quality of the coke as a final product becomes small. Therefore, even in case of coal unsuitable for the production of coke for blast furnace, it may be blended only in a small amount, and serves to stabilize the quality of coke as a merit.

As to the raw coals blended for the production of coke for blast furnace, however, it is presently used to select only coals having relatively good quality as

compared with coal used for the production of generalpurpose coke. Therefore, the iron-making technicians are always troublesome in the saving of good quality coals as it is.

Among the raw coals being cheap and available in a greater amount, for instance, there is medium coking coal having a high content of inert component indicating an mean reflectance of 0.9~1.1 and a maximum fluidity of not more than 3.0. And also, such raw coals indicate substantially the same quality property as in the above usual coal blend. According to the inventors' study, however, when a greater amount of this raw coal is blended and carbonized, the desired coke strength can not actually be obtained though the quality is similar to that of the coal blend, and hence it is obstructed to use it in a greater amount.

On the other hand, according to the conventional method of blending many kinds of raw coals having a certain quality, e.g. about 20 brands of coals must be always stocked in a coal yard, so that there are problems that the yard site is ensured and the cost for unpacking and quarrying becomes expensive and the like.

In the conventional technique, it is required to adjust and blend many brands of raw coals as a coal blend to be charged into the coke oven as mentioned above. However, the raw coal to be blended is difficult to get in accordance with the brand thereof, or even if such raw coals are get, there is a problem in the maintenance of the raw coals in the stock yard.

Under the above circumstances, it is, therefore, an object of the invention to propose a method of advantageously producing coke for metallurgy having an excellent quality such as strength and the like as compared with the conventional method, particularly high-strength coke capable of using in a large-size blast furnace by blending a greater amount of a brand of a raw coal being cheap and easily available with several brands of raw coals.

#### DISCLOSURE OF INVENTION

The inventors have made various studies with respect to the kinds of raw coals and the blending thereof in order to achieve the above object and found that there is a combination suitability or affinity in a combination of so-called particular brands of raw coals because the coke strength is largely shifted from that estimated from a weighted mean value of each raw coal in accordance with the method of combining raw coals of different production countries (each brand coal). That is, it has been confirmed that the strength required as a coke for metallurgy is obtained by utilizing the affinity of particular brands of raw coals with other brand of raw coals even if the raw coal is restricted to few brands and these brands are blended, and as a result the invention has been accomplished.

That is, the invention lies in a method of producing coke for metallurgy by blending plural brands of raw coals to form a coal blend and carbonizing it in a coke oven, characterized in that a coal blend containing not less than 60 wt% of medium coking coal having a content of inert component of not less than 30%, a middle coalificiation degree and a low fluidity is used as a coal charged into the coke oven.

In the invention, the above medium coking coal of middle coalification degree and low fluidity is favorable to have a equilibrium moisture content of not less than 3.5%.

In the invention, it is favorable that the coal blend consists of 60~95 wt% of the medium coking coal having the middle coalification degree and low fluidity and 5~40 wt% of hard coking coal and/or medium coking coal having a high coalification degree and/or a middle-high fluidity.

In the invention, it is favorable that one or more

raw coals having an mean reflectance  $(R_0)$  as the coalification degree of 0.9~1.1 and a maximum fluidity (MF) as a coking property of not more than 3.0 are used as the medium coking coal having the middle coalification degree and low fluidity.

In the invention, it is favorable that either one or more of high coalification coking coal having an mean reflectance  $(R_0)$  as the coalification degree of not less than 1.3 and middle-high fluidity coking coal having a maximum fluidity (MF) of not less than 3.0 are used as the hard coking coal and/or medium coking coal having the high coalification degree and /or middle-high fluidity.

In the invention, the product coke is favorable to indicate of a tumbler strength (TI<sub>6</sub>) of not less than 83%.

According to the method of the invention having the above construction, raw coals being cheap and available in a great amount can be blended in a greater amount, so that it is possible to stably ensure coke for a large-size blast furnace having an excellent quality indicated by TI<sub>6</sub> of not less than 83%, preferably not less than 84% even when the coal blend is formed by blending raw coals of brands smaller than the conventional brand number.

#### BRIEF DESCRIPTION OF DRAWINGS

Fig. 1 is a graph showing properties of middle coalification and low fluidity coal and general-purpose coal blend.

Fig. 2 is a graph showing an influence of blending ratio of middle coalification and low fluidity coal and a hard coking coal upon coke strength (tumbler strength).

Fig. 3 is a graph showing a relation between blending ratio of middle coalification and low fluidity coal and coke strength.

Fig. 4 is a graph showing a relation between blending ratio of middle coalification and low fluidity coal and coke strength when blending two middle

coalification and low fluidity coals having similar properties.

#### BEST MODE FOR CARRYING OUT THE INVENTION

An embodiment of the invention will be described in detail with the course developing the invention below.

Fig. 1 is a graph showing indicating qualities of main brands of raw coals (64 brands) imported in Japan at the present time, wherein an abscissa is a coalification degree  $R_0$  of coal (as  $R_0$  becomes higher, the coke strength in the carbonization increases) and an ordinate is a fluidity MF of coal (indication of coking property of coal).

At the present time, as a coal blend charged into an coke oven,  $10\sim20$  brands of raw coals among raw coals imported in Japan are blended so as to adjust the properties to coalification degree  $R_0 = 0.9\sim1.2$  and fluidity MF = about  $2.3\sim3.0$ .

For instance, the inventors have particularly noticed the particular brands of raw coals and found that medium coking coal having a middle coalification degree and a low fluidity (hereinafter referred to as middle coalification-low fluidity coal) tested is shown by black circle in Fig. 1 and is approximately equal to a grade of coal blend having a coalification degree  $R_0$  = 1.05 and a fluidity MF = 2.4 (charging coal). This means that it is possible to blend a greater amount, for example, not less than 50% of such a middle coalification-low fluidity coal. According to the inventors' studies, however, it has been confirmed that when the middle coalification and low fluidity coal is merely blended in a greater amount, the coke strength considerably lowers and is unsuitable as the coke for metallurgy. As a result of searches, there are considered various causes that the equilibrium moisture content in the total water content of 7.5% is as high as not less than 3.5% (usual raw coal is about 2.5%) and the like. Among them, it has been confirmed that a maximum

cause lies in a point that the inert component such as fusinite, semi-fusinite or the like as a coal structure component is 10~less than 30% in the usual raw coal and as high as 40~50 wt% in the middle coalification and low fluidity coal.

For this end, the inventors expect the "affinity" as a blending property of the coals and examined on the combining affinity of the middle coalification and low fluidity coal with the other brands of reinforcing coking coals, particularly hard coking coal and medium coking coal. That is, various coal blends are prepared by blending the middle coalification and low fluidity coal with several kinds of strength-reinforcing coking coals shown in Table 1 and the coal blends are subjected to carbonization test in an coke oven.

As a result, it has been confirmed that the coke strength (tumbler strength) required as a coke for metallurgy is obtained when the blending ratio of the middle coalification and low fluidity coal to the strength reinforcing coal of other brand (hard, medium coking coal) is within a range of 60-40-95/5 as shown in Fig. 2.

Fig. 2 is a graph showing an effect of improving the tumbler strength TI<sub>6</sub> when the strength of the coke made from only the middle coalification and low fluidity coal is zero, which shows a comparison the strength of coke made from only the middle coalification and low fluidity coal and the tumbler strength of two coal blend obtained by blending the middle coalification and low fluidity coal and the other brand of strength-reinforcing coking coal. The numerical value in the figure shows a blending ratio of the middle coalification and low fluidity coal and the other brand coal.

Moreover, the tumbler strength as a strength of coke is indicated by a value as measured on an amount of not less than 6 mm after a sample is rotated at 400 revolutions using a tumbler strength testing machine

#### described in JIS K2151 and then screened.

(Table 1)

Brand of Coal		Mean reflectance R <sub>0</sub>	Maximum fluidity MF	Tumbler strength $^{*}$ $\triangle$ TI $_{6}$ (%)
Middle coalification and low fluidity coal (X-coal)		1.05	2.40	-
	A	1.59	1.63	1.1
	В	1.57	1.42	0.9
Reinforcing	С	1.46	2.37	0.7
coals	D	1.38	1.22	0.5
	E	1.23	1.60	0.3
	F	1.14	4.08	0.2

<sup>\*)</sup> $\triangle$ TI<sub>6</sub>: Change of tumbler strength when a blending ratio of X coal/i coal (i=A~F) is 95/5

As mentioned above, it has been confirmed that when the middle coalification and low fluidity coal (X-coal) is blended with 5-40 wt% of the reinforcing coking coal (A-F) being the other brand raw coal shown in Table 1, even if the coal is blended in a greater amount, the coke strength (TI<sub>6</sub> > 83) can sufficiently be ensured and the coke strength of a target as a measure (step maintenance value) usable in a large size blast furnace of 3000-5000 m3 class is obtained. In this case, when the blending amount of the other reinforcing hard coking coal (A-F) is less than 5 wt%, the strength is lacking, while when the blending amount of the other reinforcing hard coking coal (A-F) is more than 40 wt%, the blending effect is saturated and the economical merit is lost.

And also, as the mean reflectance (coalification degree:  $R_0$ ) of the hard coking coal being the strength-reinforcing coal (A-F) becomes higher, the improving effect of the coke strength becomes higher, which means the middle coalification and low fluidity coal can be used in a greater amount. Moreover, the blending of the strength-reinforcing hard coking coal may be alone or in admixture

of plural coals because the effect to the coke strength is the same. However, when the number of coals is too large, the subject of the invention combining few brands of coals is conflicting, so that 3~4 kinds are suitable at most.

Since the hard coking coal used for the reinforcement is expensive, it is desirable to control the blending ratio of the hard coking coals in view of the cost.

For this purpose, in the invention, it is desirable that the middle coalification and low fluidity coal is blended with at least one of coking coals having a coalification degree R<sub>0</sub> larger than the mean reflectance (coalification degree) of the former coal such as high coalification hard coking coal and high coalification medium coking coal. That is, when raw coals (high coalification hard coking coal, high coalification medium coking coal) of a brand indicating a coalification degree of not less than 1.3 as a property of the coking coal is blended in an amount of 5~40 wt%, preferably about 5~20 wt%, the effect of improving the coke strength becomes remarkable.

Further, when the middle coalification and low fluidity coal is blended with 5~40 wt%, preferably 5~20 wt% of middle-high fluidity hard coking coal or medium coking coal indicating maximum fluidity MF larger than the maximum fluidity MF of the former coal or MF value of not less than 3.0, the coke strength can be surely increased. This may be also used in the blending of the above high coalification coking coal.

As mentioned above, according to the invention, it is said that it is favorable to blend the middle coalification and low fluidity coal with hard coking coal or medium coking coal having high coalificiation degree and/or middle coalification degree as a raw coal for the reinforcement of the coke strength.

As the middle coalification and low fluidity coal, the production country and production area are not

particularly restricted, and use may be made of ones similar to coal having large inert component and equilibrium moisture content and the aforementioned properties. That is, as shown in Table 2, Y-coal as a raw coal similar to the properties of the middle-coalification and low fluidity coal is a coal having similar properties except that volatile matter (VM) and maximum fluidity (MF) are slightly high and the mean reflectance (R<sub>0</sub>) is slightly low. Such raw coals are coals being difficult to use in the conventional blending method likewise the aforementioned middle coalification and low fluidity coal. However, Y-coal can be applied to the blending of few brands of raw coals likewise the above middle coalification and low fluidity coal.

Moreover, the raw coals having similar properties (Y-coal etc.) may be used together because the mean reflectance ( $R_0$ ) is within a range of 0.9~1.1 and the maximum fluidity (MF) is not more than 3.0 likewise the middle coalification and low fluidity coal.

(Table 2)

	Volatile Fixed Total			1 1	Mean	Maceral analysis		
Brand	matter	carbon	sulfer content	fluidity	reflect- ance	Vitrinite	Semi- fusinite	Fusinite
	VM	FC	TS	MF		(Vt)	(SF)	(F)
X-coal (middle coalification and low fluidity coal)	27.1	65.7	0.43	2.420	1.073	51.0	46.0	1.5
Y-coal	28.7	62.8	0.40	2.780	1.044	56.0	33.6	5.2

## Example 1

As the middle coalification and low fluidity coal as a main raw material is used X-coal shown in Table 3, and A-coal is used as an example of high coalification coking coal used for the reinforcement of the strength, and C-coal is used as a medium coking coal or hard coking coal indicating an mean reflectance higher than that of middle

coalification and low fluidity medium coking coal. A coal blend for charge into a coke oven is prepared by blending them at a ratio of X-coal:A-coal:C-coal = 81:9:10. The properties of each of these coals are shown in Table 3.

(Table 3)

Brand	Volatile matter	Ash content	Fixed carbon	Total sulfer content	Crucible swelling index	Maximum fluidity	Mean reflect- ance
	VM	Ash	FC	TS	CSN	MF	R <sub>0</sub>
X-coal (middle coalification and low fluidity coal)	27.1	7.2	65.7	0.43	6	2.42	1.073
A-coal	18.3	9.3	72.4	0.21	9	1.505	1.588
C-coal	28.1	9.1	62.8	0.67	7	3.959	1.117

And also, Fig. 3 shows an influence of the blending ratio of the middle coalification and low fluidity coal upon the strength. As shown in the figure, when the blending ratio of coal blend blending the middle coalification and low fluidity coal is increased, the strength (TI<sub>6</sub>) gradually lowers as shown by a as compared with the coke strength of usual coal blend (TI<sub>6</sub> = 84.4%), but the strength is obtained at a level approximately equal to that of the usual coal blend in case of the above blending ratio (X-coal:C-coal:A-coal = 81:10:9) as shown by b.

In the production method of coke for metallurgy blending a greater amount of the middle coalification and low fluidity coal, it is favorable to use black water coal produced in Australia as the middle coalification and low fluidity coal.

## Example 2

A coal blend is prepared by using X-coal of Table 2 and Y-coal of Table 2 having properties similar to those of X-coal as plural middle coalification and low fluidity coals being main raw material, A-coal in Table 3 as an

example of high coalification coking coal used for reinforcing strength, and C-coal in Table 3 as an example of meidum coking coal or hard coking coal indicating an mean reflectance larger than that of middle coalification and low fluidity medium coking coal, and blending them at a ratio of X-coal:Y-coal:A-coal:C-coal = 81-y:y:9:10 (y = 0~81).

The test results of mixing X-coal and Y-coal are shown in Table 4. It is possible to mix and use Y-coal with the middle coalification and low fluidity coal having a maximum fluidity (MF) of not less than 3.0 when the mean reflectance ( $R_0$ ) is within a range of 0.9~1.0. Example 3

An operation experiment is carried out by using cokes obtained from the coal blends blending a greater amount of the middle coalification and low fluidity coal according to the invention in Examples 1 and 2 and charging into a blast furnace. The use results are shown in Table 4. In this case, the increase of permeation resistance is somewhat observed in the lower portion of the furnace, but there is no problem in the operation of the blast furnace.

## (Table 4)

Evaluation items		①Blen grea luation items of m coal low		②Usual coke	①-②	Evaluation
	Air permeat △P/V	ion	0.252	0.254	-0.002	-
			29.3	31.3	-2.0	
Operation of blast furnace	Index of permeation resistance F2M  Lower portion F2L	portion	34.6	36.0	-1.4	-
		167.8	162.9	+4.9	- (△)	
	Fuel ratio (kg/t)		493.5	496.0	-2.5	(O)
Quality of molten	Tapping (S)		0.0193	0.0242	-0.0049	000
iron	Tapping (Si	)	0.263	0.263	±0	- (△)

## INDUSTRIAL APPLICABILITY

As mentioned above, according to the invention, it is possible to produce coke for large size blast furnace by adopting coal of middle coalification degree and low fluidity having a large inert component, which could not be used in the conventional method of blending a few of each many brands of raw coals in the conventional coke production for blast furnace, and blending great amount of few brands of raw coals. As a result, there can be produced coke for metallurgy in a cheap cost.

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#### **CLAIMS**

- 1. A method of producing coke for metallurgy by blending plural brands of raw coals to form a coal blend and carbonizing it in a coke oven, characterized in that a coal blend containing not less than 60 wt% of medium coking coal having a content of inert component of not less than 30%, a middle coalificiation degree and a low fluidity is used as a coal charged into the coke oven.
- 2. A method of producing coke for metallurgy according to claim 1, wherein the medium coking coal of middle coalification degree and low fluidity has a equilibrium moisture content of not less than 3.5%.
- 3. A method of producing coke for metallurgy according to claim 1 or 2, wherein one or more coals having an mean reflectance  $(R_0)$  as a coalification degree of 0.9~1.1 and a maximum fluidity (MF) as a coking property of not less than 3.0 are used as the medium coking coal of middle coalification degree and low fluidity.
- 4. A method of producing coke for metallurgy according to claim 1, wherein the coal blend consists of 60~95 wt% of the medium coking coal having the middle coalification degree and low fluidity and 5~40 wt% of a high coalification hard coking coal and/or a high coalification medium coking coal having a coalification degree higher than that of the above coal.
- 5. A method of producing coke for metallurgy according to claim 1, wherein the coal blend consists of 60~95 wt% of the medium coking coal having the middle coalification degree and low fluidity and 5~40 wt% of a middle-high fluidity hard coking coal and/or a middle-high fluidity medium coking coal having a maximum fluidity MF larger trhan that of the above coal.
- 6. A method of producing coke for metallurgy according to claim 4, wherein the high coalification hard coking coal and medium coking coal are coals having an mean reflectance  $(R_0)$  as the coalification degree of not less

## than 1.3.

- 7. A method of producing coke for metallurgy according to claim 5, wherein the middle-high fluidity coking coal and medium coking coal are coals having a maximum fluidity (MF) of not less than 3.0.
- 8. A method of producing coke for metallurgy according to any one of claims 1~7, wherein the coke as a product has a tumbler strength (TI<sub>6</sub>) as a strength of not less than 83%.

#### ABSTRACT

In a method of producing coke for metallurgy by carbonizing a coal blend obtained by blending plural raw coals in an coke oven, a coal blend containing not less than 60 wt% of a medium coking coal of middle coalification degree and low fluidity having an inert component content of not less than 30% is used as a coal charged into the coke oven, whereby a great amount of raw coal of a brand being cheap and easily available can be blended in a great amount and hence coke for metallurgy having an excellent quality such as strength or the like can be produced by blending few brands of coals as compared with a coal blend of many brands.

Fig.1

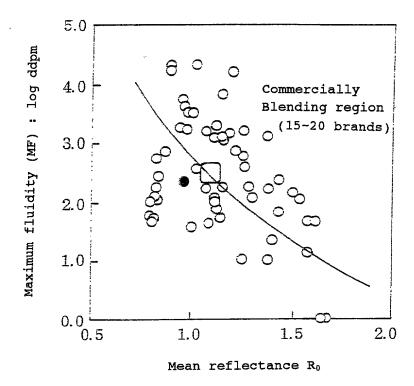


Fig.2

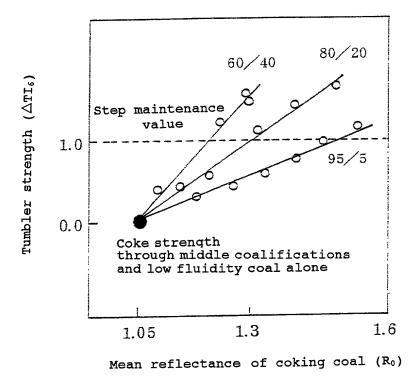
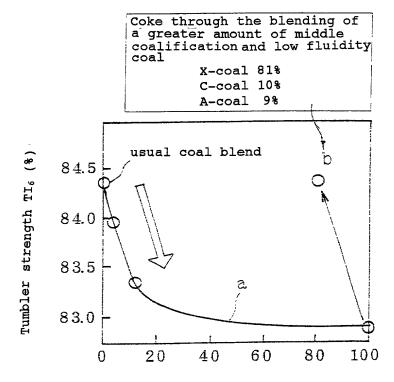
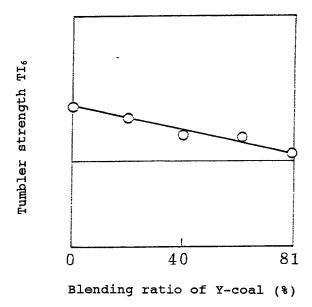


Fig.3



Blending ratio of middle coalification and low fluidity coal (%)

Fig.4



,	Express Mail Label EL525816371US  Attorney Docket No.1034-00
	Original Application
	PCT National Application U.S. Designated Office
	Continuation or Divisional Application
	Continuation-in-Part Application
	COMBINED DECLARATION, POWER OF ATTORNEY AND PETITION
As a	below named inventor, I hereby declare that:
My r	esidence, post office address and citizenship are as stated below next to my name,
I beli inven the in	eve I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint tor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on vention entitled METHOD OF PRODUCING COKE FOR METALLURGY
	hich is described in the specification and claims
	attached hereto.
: • *}	☐ filed on
	Application Serial No.
; ;	and was amended on
	(if applicable)
:. <b>I</b> V	hich is described in International Application No. <u>PCT/JP99/04058</u>
	d July 28, 1999 and as amended on
.i	(if any),
whic	n I have reviewed and for which I solicit a United States patent.
I here	by state that I have reviewed and understand the contents of the above-identified specification, including the claims, nended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to the examination of this application in accordance with Title 37, Code of Federal Regulations, §1.56.

I do not know and do not believe that this invention was ever known or used in the United States before my or our invention thereof or patented or described in any printed publication in any country before my or our invention thereof or more than one year prior to this application or said international application, or in public use or on sale in the United States of America more than one year prior to this application or said international application, or that the invention has been patented or made the subject of an inventor's certificate issued before the date of this application or said international application in any country foreign to the United States of America on an application filed by me or my legal representatives or assigns more than twelve months prior to this application or said international application, or that any application for patent or inventor's certificate on this invention has been filed in any country foreign to the United States of America prior to this application or said international application by me or my legal representatives or assigns except as identified below.

## COMBINED DECLARATION, POWER OF ATTORNEY AND PETITION (Page 2)

Attornev	Docket No.	1034-	0.0
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I hereby claim foreign priority benefits under Title 35, United States Code, §119(a)-(d) or §365(b) of any foreign application(s) for patent or inventor's certificate, or §365(a) of any PCT International Application which designated at least one country other than the United States of America, listed below and have also identified below any foreign application(s) for patent or inventor's certificate or of any PCT International Application having a filing date before that of the application on which priority is claimed:

Number	Country	Date of Filing (day,month,year)	Priority Claimed
10/214092	Japan	29 Jul. 1998	
			□ yes □ no
			□ yes □ no
			□ yes □ no
			□ yes □ no
PCT International Ap	oplication(s) in the manne	r provided by the first paragraph o	lisclosed in the prior United States of Title 35, United States Code, §112  (Status) (patented, pending, abandoned)
(Application Serial N	lo.) (Fili	ng Date)	(Status)(patented,pending,abandoned
022469 and the follow		to prosecute this application and tra	attorneys listed under Customer No ensact all business in the United States
T. Daniel Christenbu Guy T. Donatiello Paul A. Taufer James A. Drobile Austin R. Miller	Reg. No. 31,750 Reg. No. 33,167 Reg. No. 35,703 Reg. No. 19,690 Reg. No. 16,602	Patrick J. Farley Michael A. Patané David A. Sasso Robert A. McKinley Sharon Fenick	Reg. No. 42,524 Reg. No. 42,982 Reg. No. 43,084 Reg. No. 43,793 Reg. No. 45,269
Gerard J. Weiser Joan T. Kluger	Reg. No. 19,763 Reg. No. 38,940	Stewart M. Wiener	Reg. No. 46,201
SEND CORRESPO	ONDENCE TO:	DIRECT TELEPHO ATTORNEY OF RI	

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Schnader Harrison Segal & Lewis 36th Floor, 1600 Market Street

Philadelphia, PA 19103

# COMBINED DECLARATION, POWER OF ATTORNEY AND PETITION (Page 3)

Attorney Docket No. 1034-00

I hereby petition for grant of a United States Letters Patent on this invention.

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

1. FULL NAME OF SOLE OR FIRST INVENTOR	INVENTOR'S SIGNATURE	DATE
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# **▼** COMBINED DECLARATION, POWER OF ATTORNEY AND PETITION (Page 4)

Attorney Docket No. 1034-00

8. FULL NAME OF SOLE OR FIRST INVENTOR		OR'S SIGNATURE	DATE Q /2	
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RESIDENCE	CITIZE	NSHIP		
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11. FULL NAME OF ADDITIONAL JOINT INVENTOR, IF ANY		INVENTOR'S SIGNATURE	DATE	
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